

Process Development for Hydrometallurgical Recovery of Base and Precious Metals from Waste Printed Circuit Boards

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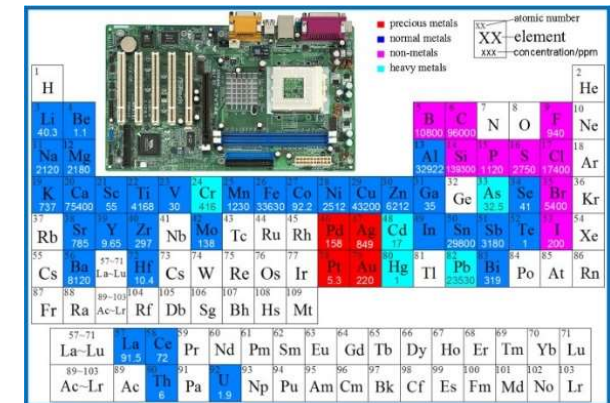
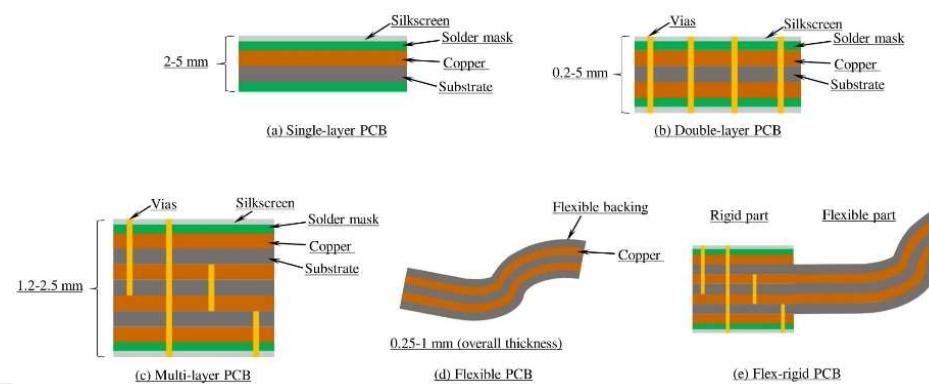
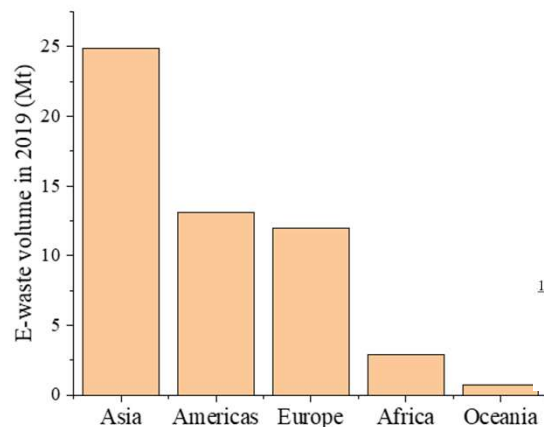
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Outline

1. “Urban Mining” of e-waste
2. Development of glycine-based process
3. Development of sulfuric acid leaching process
4. Recommendations for future study
5. Acknowledgements

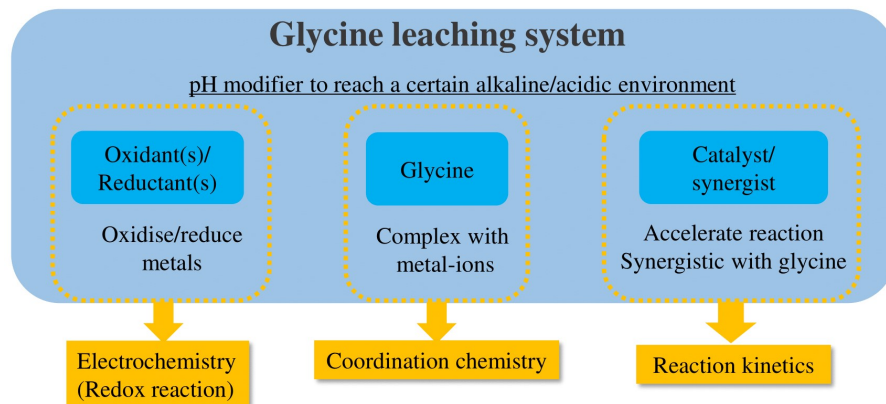
“Urban Mining” of e-waste

- Australia generated 554 kt of e-waste in 2019, ranking 5th worldwide per capita, and only 10.4% of them were documented to be collected and recycled.
- Waste PCBs are complicated e-waste in composition and contents: 40% metals, 30% plastics, 30% ceramics; ~40 types of metals and ~10 types of non-metals; metals locked in plastics & alloys.
- Proximity to the urban area – requiring a safe process.



“Urban Mining” of e-waste

- Western Australia’s scenario
 - Low e-waste volume – a pyrometallurgical process may not be highly economical
 - Vast geography – expensive road transport to a centralized location
- Why hydrometallurgy?
 - De-centralized; flexible in scales and modules; capital-friendly to SMEs
- Glycine leaching systems
 - Involving technologies invented at Curtin University and owned by Draslovka a.s.



Waste PCBs



Mechanical-physical processing



Pyrometallurgy

- Incineration
- Pyrolysis

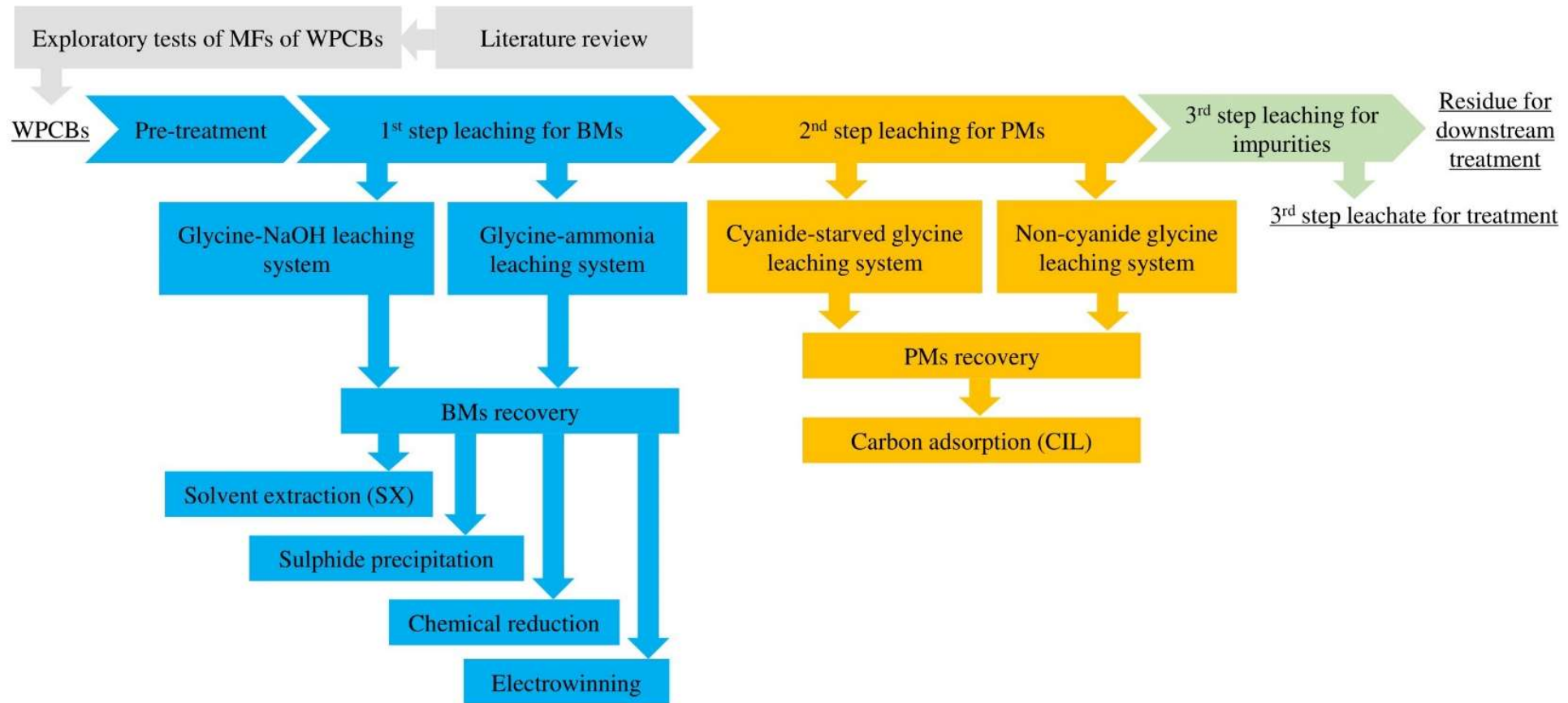
Hydrometallurgy

- Mineral acid
- Organic acid
- Ammonia
- Cyanidation
- Thio-system

Bio-metallurgy (bioleaching)

Development of glycine-based process

- Schematic diagram of process development



Development of glycine-based process

■ Publications from glycine-based process development



Review
Hydrometallurgical recovery of metals from waste printed circuit boards (WPCBs): Current status and perspectives – A review

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An Alkaline Glycine-Based Leach Process of Base and Precious Metals from Powdered Waste Printed Circuit Boards

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Abstract

Electronic waste (E-waste) is a growing problem. It contains a variety of metals, including base and precious metals. In addition, toxic substances are present in the plastic substrates. E-waste recycling processes are still in the early stages of development. This paper presents a new alkaline glycine-based leach process for the recovery of base and precious metals from powdered waste printed circuit boards (WPCBs). The process involves the use of a glycine-based leach solution to extract the metals from the WPCBs. The extracted metals are then recovered using a precipitation process. The results of the study show that the proposed process is effective in recovering base and precious metals from WPCBs. The process is also environmentally friendly and cost-effective.

Full length article

Extraction of copper and the co-leaching behaviour of other metals from waste printed circuit boards using alkaline glycine solutions

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Cyanide consumption minimisation and concomitant toxic effluent minimisation during precious metals extraction from waste printed circuit boards

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ABSTRACT

Waste printed circuit boards (WPCBs) constitute a hazardous material with up to 40 different metals, including numerous many heavy metals and environmentally harmful metals. Most hydrometallurgical processing approaches use high concentrations of toxic reagents and generate significant amounts of harmful effluents. This research investigates the use of cyanide-starved glycine solution containing no



Recovery of copper and the deportment of other base metals from alkaline glycine leachates derived from waste printed circuit boards (WPCBs)

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Extraction of precious metals from waste printed circuit boards using cyanide-free alkaline glycine solution in the presence of an oxidant

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Full length article

Development of an integrated glycine-based process for base and precious metals recovery from waste printed circuit boards

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ABSTRACT

The present study developed an integrated glycine-based process for the recovery of base and precious metals from waste printed circuit boards (WPCBs). The process involves the use of a glycine-based leach solution to extract the metals from the WPCBs. The extracted metals are then recovered using a precipitation process. The results of the study show that the proposed process is effective in recovering base and precious metals from WPCBs. The process is also environmentally friendly and cost-effective.

Review

Amino acids as lixiviants for metals extraction from natural and secondary resources with emphasis on glycine: A literature review

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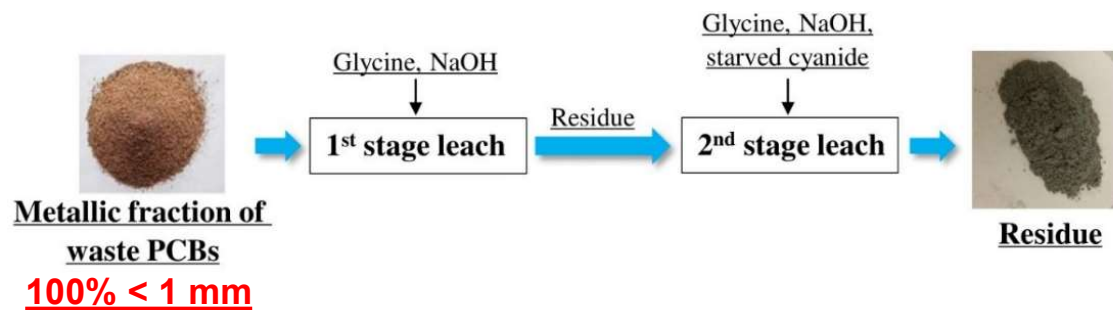
ABSTRACT

The past decade has seen significant interest in non-conventional lixiviants, particularly the growing interest in organic acids and amino acids. Of the amino acids, glycine has much coverage in the hydrometallurgical and mineral processing literature as a reagent that is non-toxic, non-volatile, and recyclable. The glycine leaching system (i.e., an aqueous system typically consisting of glycine or one of its alkali metal salts, a pH modifier, an oxidant and sometimes, other catalysts or modifiers) has been shown effective in selectively extracting base and precious metals from various resources. Using a glycine leaching system can, therefore, be considered a promising substitute for traditional methods in the hydrometallurgical industry. This paper reviews the application of amino acids and emphasizes the glycine leaching system to extract valuable metals from natural and secondary resources.



Development of glycine-based process

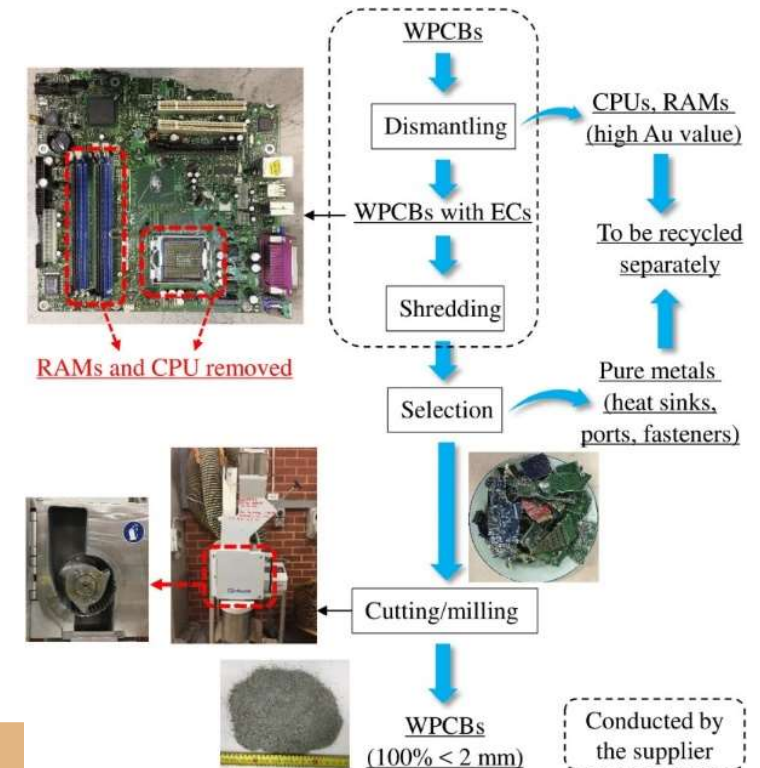
Preliminary flowsheet:



Simple pre-treatment:

- ☐ PCBs source: PC motherboards
- ☐ Electronic components remained
 - Except high-values
- ☐ No complicated physical processing

Metal content and economic value											
Metal content in wt. %							Metal content in ppm				
	Cu	Fe	Al	Sn	Pb	Zn	Ni	Co	Au	Ag	Pd
Metal content	22.60	1.83	3.18	2.81	0.34	0.69	865.50	59.72	106.77	170.50	10.37
Metal value (%)	18.2	-	0.8	6.7	0.1	0.2	0.2	0.03	66.4	1.2	6.2



Development of glycine-based process

Glycine-NaOH leaching of base metals:

- Restrained by solids%: <2-5% – waste PCBs are highly metal-rich!
- Slow leaching kinetics: ~3 days to complete copper leaching

Metals recovery from leachates:

Method	Impurity	Conditions required	Kinetics	Co-precipitation	Product
Hydrazine (N ₂ H ₄) reduction	None (N ₂ and H ₂ O)	pH > 12 Cu > 5g/L	>90% Cu recovery within 0.5-2 hours	Sn, Pb	Cuprite (Cu ₂ O) or metallic copper
Sulfide precipitation	Sulfur	Cu/HS ⁻ molar ratio ≤1:1.2	Fast kinetics: >90% copper recovery within 5 min	Zn, Pb, Sn, Ni	Covellite (CuS) at 87.9% purity
Solvent extraction (Mextral 54–100 and Mextral 84H)	-	15% Mextral 84H & 200 g/L H ₂ SO ₄ ; 30% Mextral 54–100 & 80 g/L H ₂ SO ₄	85-95% Cu extraction; 99% Cu stripping	Ni (Pb and Sn not investigated)	Metallic copper or copper sulfate after downstream treatment

Development of glycine-based process

Glycine-ammonia leaching of base metals:

- Solids% increased to 15%~: >40 g/L copper in PLS
- Copper leaching shortened to 24 hours
- Ammonia concentration reduced by ~80%, compared with conventional ammoniacal leaching
- Ammonia played the key roles of:
 - ✓ pH modifier
 - ✓ Synergist
 - ✓ Copper stabilizer

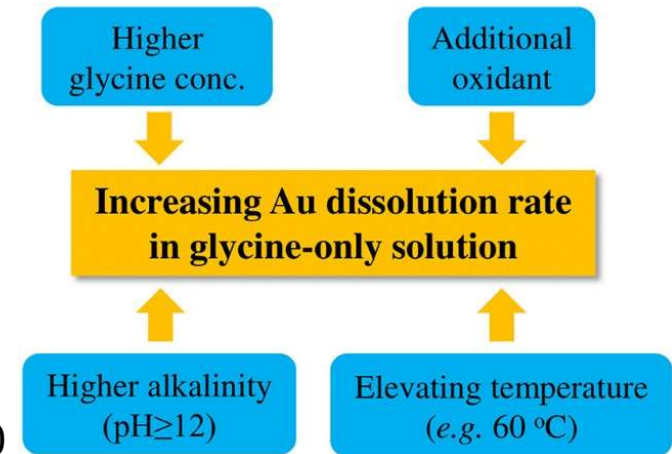
Cyanide-starved glycine leaching of precious metals:

- Cyanide acted as “catalyst” for copper and silver dissolutions
- Similar or better PMs extraction, compared with stoichiometric or intensive cyanidation
- Cyanide use was reduced by 70-90% (250 ppm vs 3500 ppm, no free cyanide after 4 hours)

Development of glycine-based process

Non-cyanide glycine leaching of precious metals:

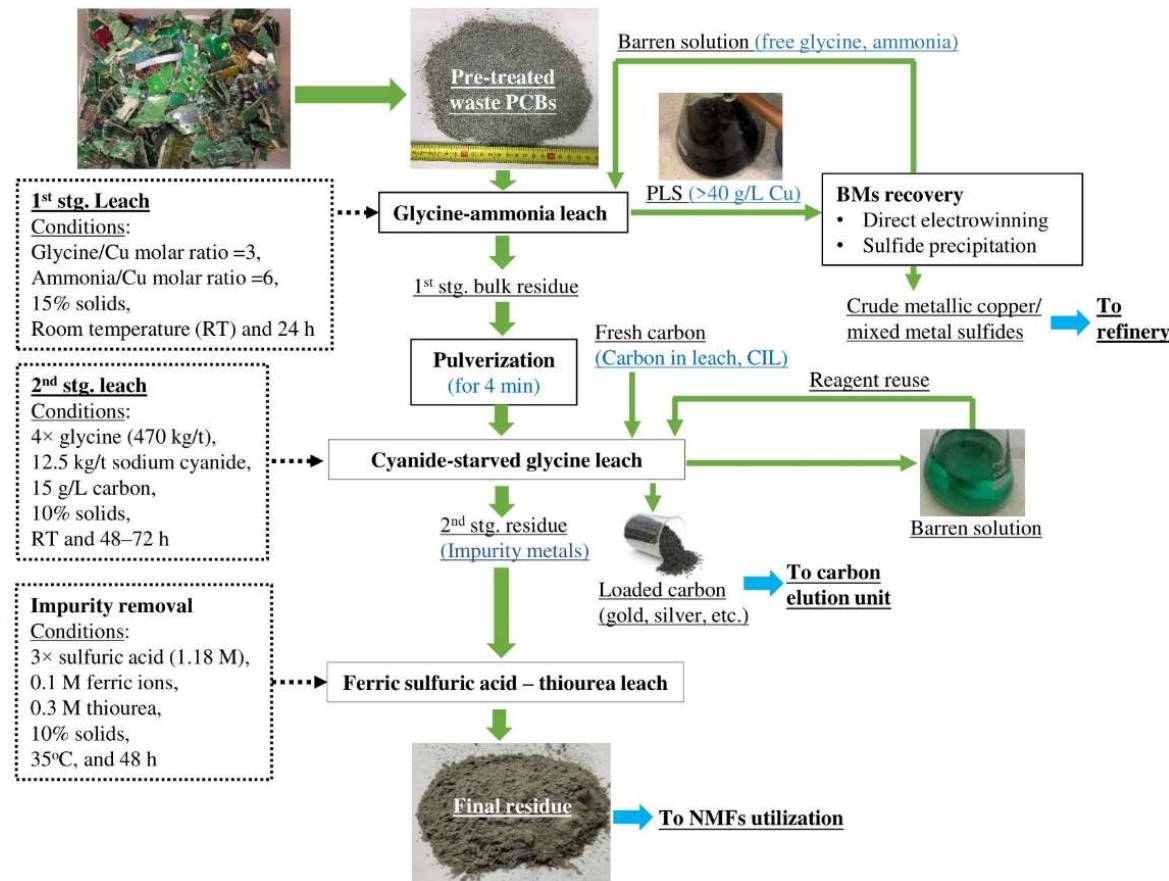
- Permanganate or ferricyanide with glycine solution effectively leached PMs, namely glycine-oxidant leaching system
- Similar or comparable PMs extraction, compared with cyanide-starved glycine leaching or intensive cyanidation
- Rapid decomposition of glycine was observed when permanganate added
- Oxidant consumptions were high, i.e., 630 kg/t K-permanganate or 610 kg/t K-ferricyanide



Development of glycine-based process

An improved process:

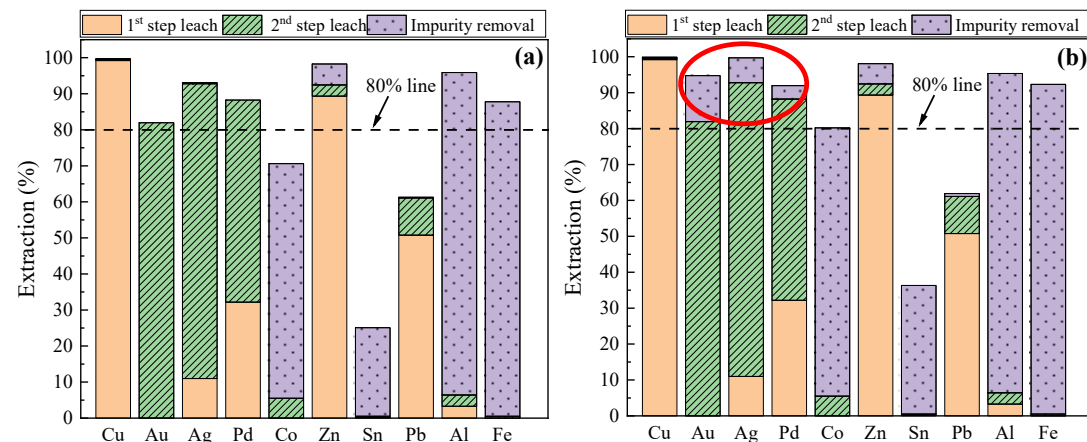
- 1st step glycine-ammonia leaching at 15% solids
- Pulverization used to liberate precious metals from plastics
- 2nd step cyanide-starved glycine leaching at 10% solids
- 3rd step sulfuric acid – Fe³⁺ – (thiourea) leaching at 10% solids



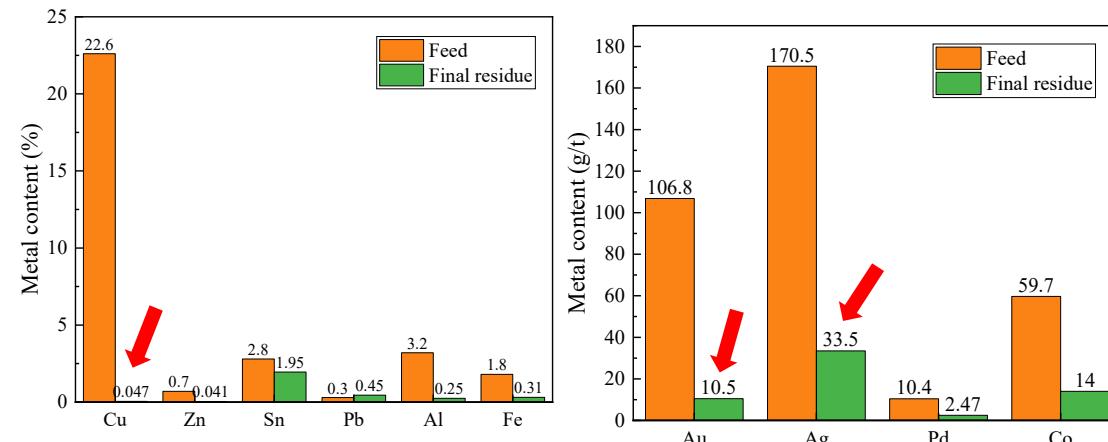
Development of glycine-based process

An improved process:

- Overall extraction: >99% copper, >90% gold, >95% silver and >85% palladium
- Metal content in residue: 0.047% copper, <1% base metals (except tin), <35 ppm precious metals



Figures above: Extraction of metals at each step of leaching, (a) without and (b) with thiourea in the 3rd step.

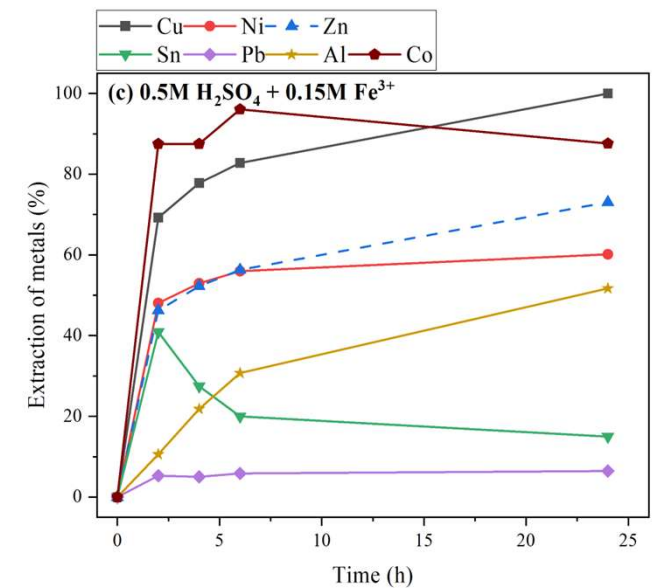
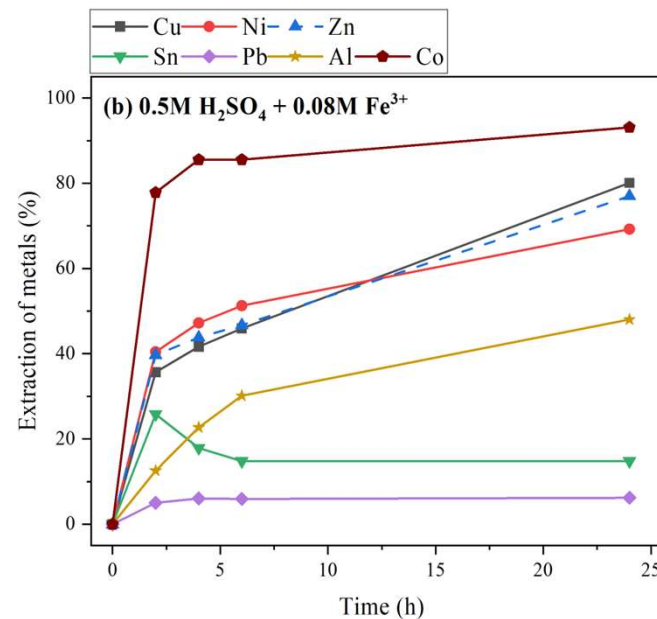
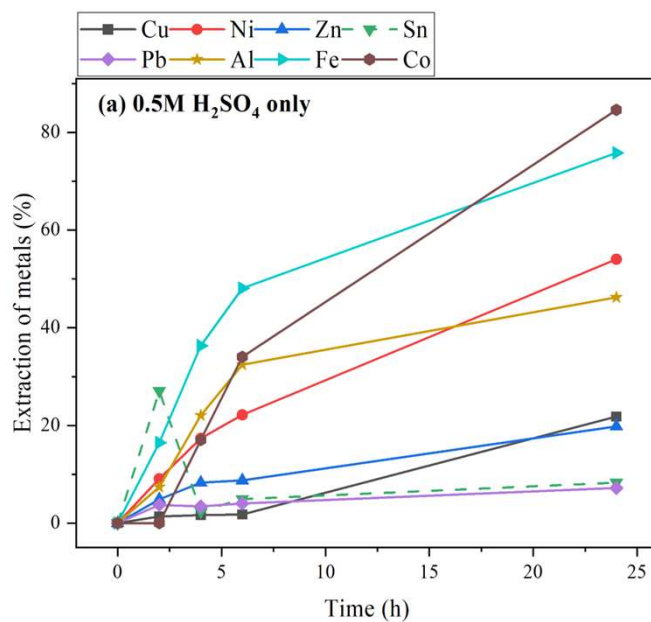


Figures above: Metal contents in the final residue after three leaching steps with thiourea in the 3rd step.

Development of sulfuric acid leaching process

Leaching of pre-treated waste PCBs (100% < 2mm):

- Oxidant, e.g., Fe^{3+} , was essential for copper leaching
- Leaching time can be shortened to ~24 hours
- Tin and lead (e.g., solder materials) remained low extractions (<20%)
- No gold and palladium were leached; silver leaching was <15%.

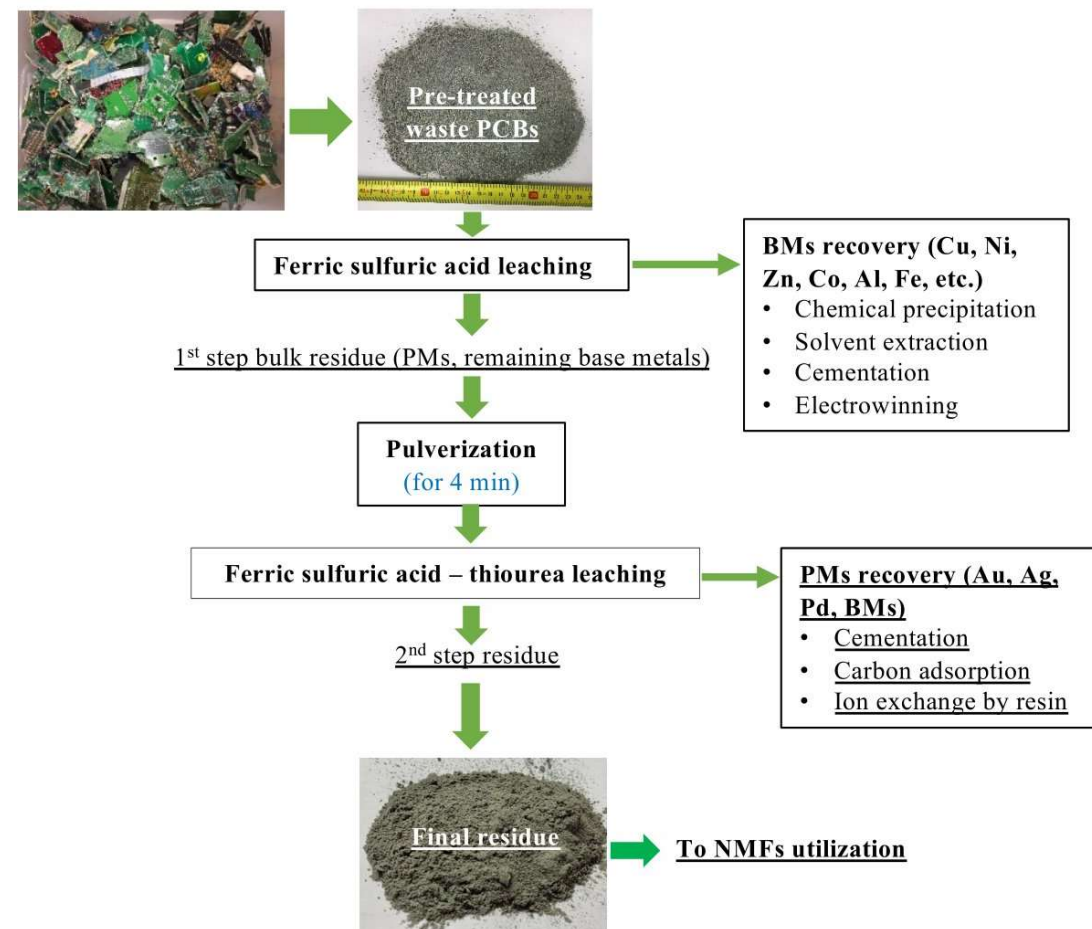


Figures above: Extraction of metals using different sulfuric acid leaching at 2% solids and room temperature.

Development of sulfuric acid leaching process

Sulfuric acid leaching process:

- Well known in chemistry
- Non-selective for base metals
- 1st step sulfuric acid – Fe^{3+} leaching of copper & base metals
- 2nd step sulfuric acid – Fe^{3+} – thiourea leaching of precious metals & remaining base metals
- Physical separation is suggested prior to hydrometallurgical leaching



Recommendations for future study

- More fundamental studies
- Mechanical-physical separation of bulk of metals
- Ferricyanide regeneration and reuse
- Glycine recycling and reuse
 - Glycine decomposition
 - Glycine quantification
- Residue utilization
- Pilot scale tests
- Techno-economic assessment

Acknowledgements



total green
recycling



Thank you for your attention!