

#### **ALTA 2023 Gold-PM Keynote Presentation**

### Chloride -

# A Precious Metals Leaching System yet to Reach its Potential

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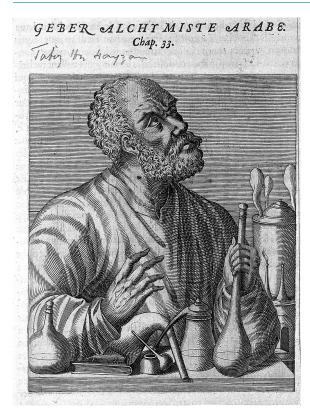
# Background

Chloride leaching of precious metals





### Discovery of Aqua Regia and Chlorine



Aqua Regia was discovered by Persian alchemist Jabir Ibn Hayyan (720-813) by the mixture of hydrochloric and nitric acids





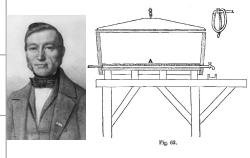
Chlorine was discovered by the Swedish chemist Carl Wilhelm Scheele (1742-1786) by the action of hydrochloric acid on manganese dioxide in 1774

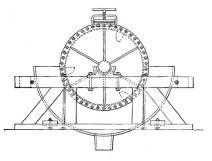


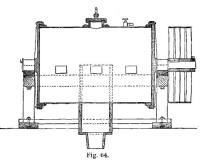


## **Early Chlorination Processes for Gold Extraction**

| Process  | Date | Pretreatment | Equipment          | Treatment  | Leach   | Recovery                      |
|----------|------|--------------|--------------------|--|---|-------------------------------|
| Plattner | 1848 | Dead roast   | Damp fixed bed vat | Cl <sub>2</sub> permeation   | Water percolation   | FeSO <sub>4</sub> reduction   |
| Duflos   | 1848 | -            | Damp fixed bed vat | In leach   | Supersaturated Cl <sub>2</sub> percolation                      | Reduction                     |
| Mears    | 1877 | -            | Rotating barrel    | Cl <sub>2</sub> 300 kPa  | Water leach   | Reduction                     |
| Thies    | 1881 | -            | Rotating barrel    | In leach   | CaOCl <sub>2</sub> /H <sub>2</sub> SO <sub>4</sub> leach 30 kPa | Reduction                     |
| Lange    | 1885 | -            | Earthenware pots   | Cl <sub>2</sub>  | Water leach   | H <sub>2</sub> S<br>reduction |
| Munktell | 1888 | Dead roast   | Damp fixed bed vat | Hot water then HCl or H <sub>2</sub> SO <sub>4</sub> for Cu/Fe removal | CaOCl <sub>2</sub> /H <sub>2</sub> SO <sub>4</sub> leach        | Lead acetate                  |







Early Processes for Generation of Chlorine:

 $2NaCl + MnO_2 + 2H_2SO_4 = Na_2SO_4 + MnSO_4 + 2H_2O + Cl_2$ 

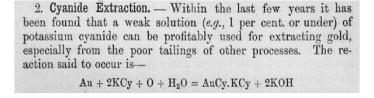
 $CaCl_2 + Ca(OCl)_2 + 2H_2SO_4 = 2CaSO_4 + 2H_2O + 2Cl_2$ 

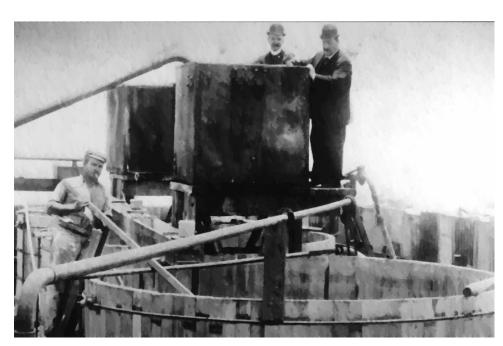




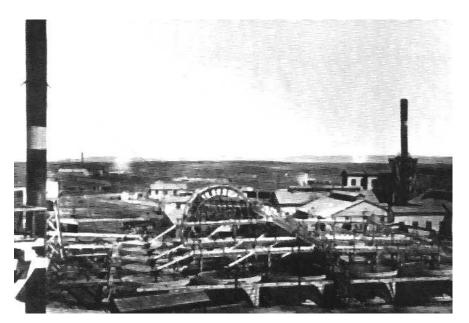
### Factors in the Replacement of Gold Chlorination by Cyanidation

- Excess chlorine losses due to volatilisation from leaky vessels
- Excess chlorine consumption due to reaction with sulphides
- Excess chlorine consumption due to reaction with base metals





Robinson GM, 1890



Simmer & Jack, 1893





# **Chemistry of Chlorination**

Precious metals leaching reactions





### **Chloride Leaching Chemistry**

#### **Gold chlorination chemistry**

 $2Au(s) + 3Cl_2(g) + 2HCl(aq) = 2HAuCl_4(aq)$ 

#### **PGM chlorination chemistry**

$$Pt(s) + Cl2(g) + 2 HCI(aq) = H2PtCl4(aq)$$

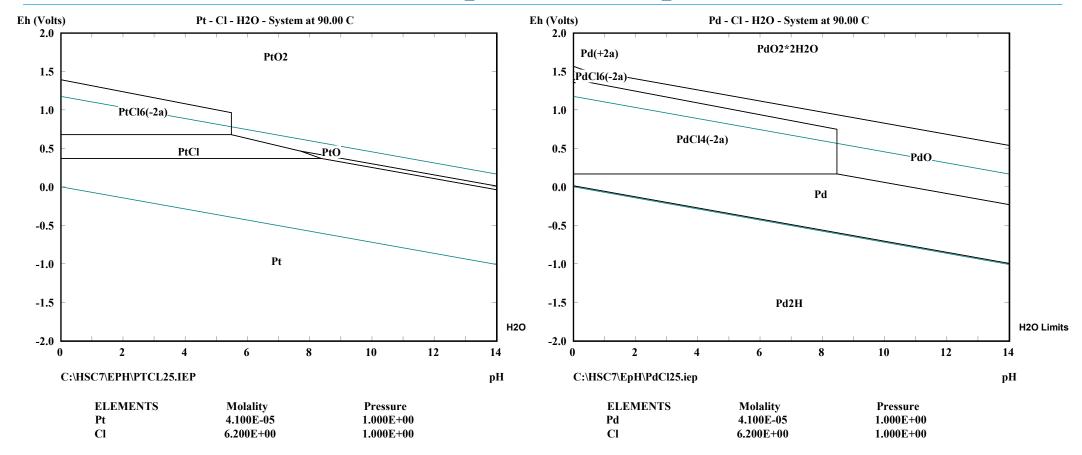
$$Pt(s) + 2 Cl_2(g) + 2 HCI(aq) = H_2PtCI_6(aq)$$

$$Rh(s) + Cl_2(g) = RhCl_2(aq)$$





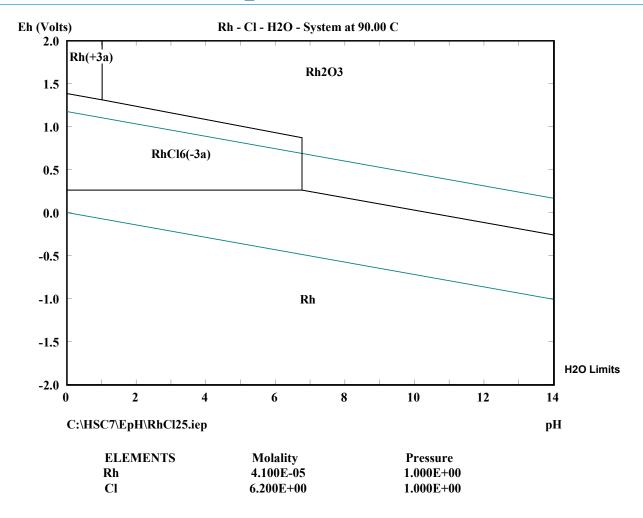
# Potential-pH Diagram for Pt-Cl-H<sub>2</sub>O and Pd-Cl-H<sub>2</sub>O Systems







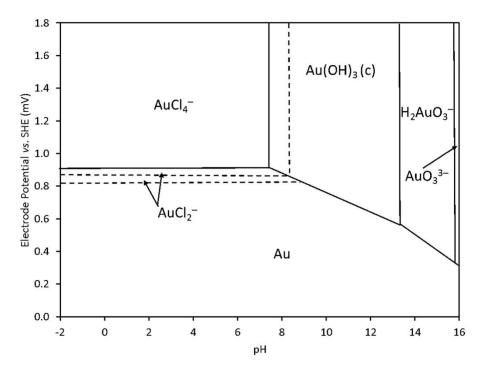
## Potential-pH Diagram for Rh-Cl-H<sub>2</sub>O System



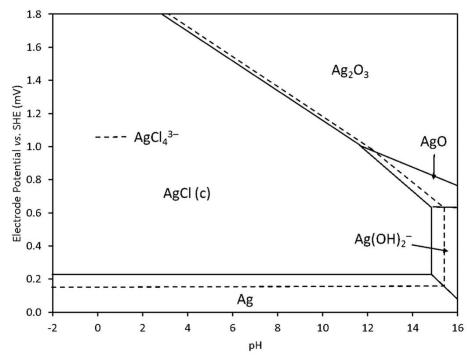




# Potential-pH Diagram for Au-Cl-H<sub>2</sub>O and Ag-Cl-H<sub>2</sub>O Systems



 $a_{\rm Au}$  = 10<sup>-3</sup> and  $a_{\rm Cl}$  = 1(solid) and = 5 (dashed); 25°C Kelsall et al., 1993



 $a_{\rm Au}$  = 10<sup>-4</sup> and  $a_{\rm Cl}$  = 1(solid) and = 2 (dashed); 25°C Welham et al., 1993





# Chloride-Based Leaching Processes

Gold and PGM recovery





# **Chloride-Based Leaching Processes for Gold**

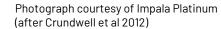
|                 |                                  |   |        | Application<br>Level           |  |
|-----------------|----------------------------------|---|--------|--------------------------------|--|
| Process         | Ligand                           | Oxidant   | Tested | 20701                          | References   |
| Hydrocopper     | CI-                              | Cu <sup>2+</sup> , O <sub>2</sub>   | D      |                                | Hyvärinen and Hämäläinen (2005), Canadian Mining<br>Journal (2006), and Infomine (2008); Lundström et al<br>(2009, 2011, 2012) |
| Intec           | Cl <sup>-</sup> /Br <sup>-</sup> | Cu <sup>2+</sup> , Fe <sup>3+</sup>   | Р      |                                | Moyles (1999), Severs (1999), and Monument Mining<br>Ltd (2016)  |
| Lifezone Metals | CI-                              | CI <sub>2</sub>   | P      | FS (2x sites,<br>South Africa) | Liddell (2009), Liddell et al. (2011),<br>Liddell and Adams (2012a,b), Adams et al. (2015,<br>2019, 2020)                      |
| N-Chlo          | Cl <sup>-</sup> /Br <sup>-</sup> | $Cu^{2+}$ , $Fe^{3+}$   | D      |                                | Nippon Mining and Metals (2008)  |
| Neomet          | CI <sup>-</sup>                  | Cu <sup>2+</sup> , Fe <sup>3+</sup><br>HNO <sub>3</sub><br>O <sub>2</sub><br>H2O2 | Р      |                                | Harris and White (2011a,b, 2013)   |
| Nichromet       | Cl <sup>-</sup> /Br <sup>-</sup> | Cl <sub>2</sub> /Br <sub>2</sub>  | Р      |                                | Lalancette (2009), and Lemieux et al. (2014)   |
| Outotec         | Cl <sup>-</sup> /Br <sup>-</sup> | Cu <sup>2+</sup> , Fe <sup>3+</sup>   | Р      |                                | Miettinen et al. (2013)  |
| Platsol         | CI <sup>-</sup>                  | 02  | Р      | FS (Northmet,<br>USA)          | Ferron et al. (2000, 2003), Wardell-Johnson et al. (2009), Dreisinger et al (2016)   |



### **Chlorination in Platinum Refineries**

A heated agitated 2.2 m<sup>3</sup> titanium vessel for batch dissolution of a PGM concentrate via intermittent chlorine sparging









# **Platinum-Group Metals Refineries**

| Parameter                    | Unit | Lonmin                    | Kratsvetmet                        | Vale Acton                           | JM/Anglo                   | Impala                |
|------------------------------|------|---------------------------|------------------------------------|--------------------------------------|----------------------------|-----------------------|
| Main feed material           |      | Leached<br>matte          | Anode slime                        | Concentrate/<br>Catalyst/<br>E-Waste | Leached mag<br>concentrate | Leached matte         |
| HCI                          | g/L  | 219                       | 175                                |                                      |                            | 109                   |
| Temperature                  | С    | 65                        | 70                                 | 90-98                                | 120                        | 65-70                 |
| Pressure                     | bar  | 1                         | 3                                  | 1                                    | 4                          | 0.7                   |
| Residence time               | h    | 6                         | 2                                  |                                      |                            | 8                     |
| Material                     |      | Glass-lined               | Ti                                 |                                      |                            | Ti Gr2; jacketed      |
| Volume                       | m3   | 2.2                       | 1                                  |                                      |                            | 2.5                   |
| Impeller                     |      | Pitched-<br>blade turbine | Hollow shaft inductor              |                                      |                            | Pitched-blade turbine |
| Free Cl <sub>2</sub> removal |      | Air sparging              |                                    |                                      |                            | "Dechlorinated"       |
| Gold recovery<br>method      |      | N2H4<br>reduction/HCI     | Precipitate<br>with<br>concentrate | SX                                   | SX                         | IX                    |
| Gold product                 |      | Crude gold                | 99.99% Au                          | 99.99                                | 99.95                      | 99.95                 |
| Typical gold recovery        | %    | 99                        | 98                                 | 99                                   | 99.5                       | 94                    |
| First-pass yield             | %    | 92                        |                                    | 98                                   | 84                         | 98                    |





# Lifezone Metals

Gold and PGM Hydromet Processing

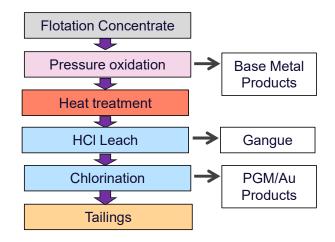




### Lifezone Metals Hydromet - Overcoming the Chlorination Limitations

#### The globally patented hydrometallurgical Lifezone Metals Process:

- *Chlorine losses* due to volatilisation
  - <u>minimised</u> via properly engineered vessels
- Chlorine consumption due to reaction with sulphides and base metals
  - <u>eliminated</u> via prior removal of these reagent consumers by pressure oxidation
- Gas-liquid-solid contact constraints in static and rolling reactors
  - <u>eliminated</u> by use of modern CSTR reactors
- Refractory, complex and deleterious PGM-Au-gangue mineral phases
  - <u>eliminated</u> by heat treatment conditioning and preleach prior to chlorination







#### Lifezone Metals Hydromet Process Background

#### The globally patented hydrometallurgical Lifezone Metals Process:

- Developed for the extraction of platinum group metals (PGM), gold, silver and base metals from PGM sulphide flotation concentrates without smelting or cyanidation
- Successfully demonstrated on various PGM and polymetallic concentrates, including UG2, Merensky, Platreef and Great Dyke from southern Africa and polymetallic concentrates from North America, Australia and Africa.
- High recoveries (94 % 99 %) for selective extraction of a range of value metals, including precious metals (Pt, Pd, Rh, Au, Ag) and base metals (Ni, Co, Cu, Zn, Sn, Pb, Mo) with stabilization of impurities such as As and S without gaseous emissions.
- KellGold process variation for refractory gold, Cu/Au and preg-robbing gold concentrates, enabling production of refined metals at the mine site without the use of cyanide
- Licensed as Kell Process in SADC region via KellTech Ltd, along with shareholders Sedibelo Platinum and IDC (Industrial Development Corporation of South Africa)





### Lifezone Metals Hydromet - Technical Features

Patented process comprising four basic sequential steps, all of which are well proven and commonly used in the metallurgical industry and provide high recoveries of base and precious metals:

- 1. Aqueous pressure oxidation in an acidic sulphate medium to dissolve the sulphides and remove the base metals while minimising dissolution of the precious metals, producing copper, nickel and cobalt products;
- **2. Heat treatment** of the pressure oxidation residue as required, to condition the mineral phases, rendering the material amenable for subsequent leaching;
- 3. Atmospheric leaching of the iron and other gangue components in chloride media;
- **4. Atmospheric leaching of the PGM and gold** in chloride medium in a similar manner as typically used in PGM refineries, with PGM and gold recovery to high-purity products

Separate leaching stages for the precious metals and base metals:

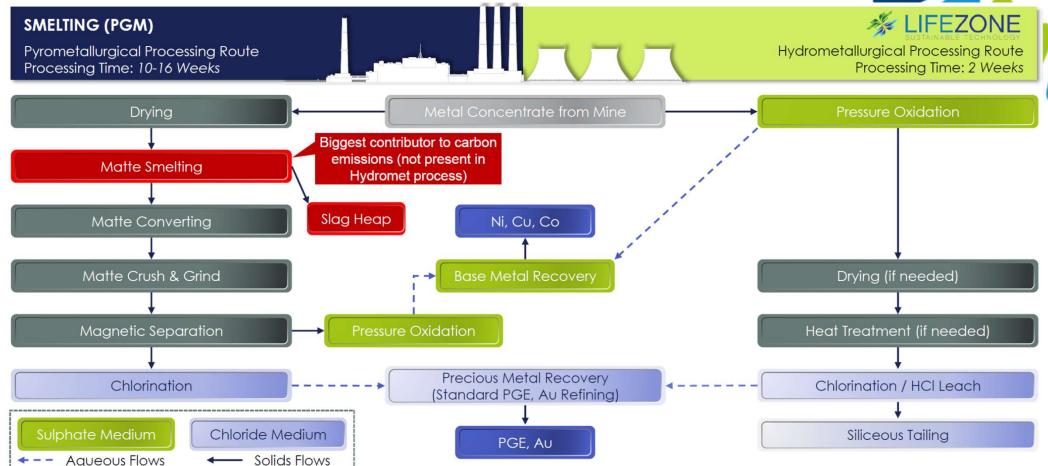
- · keeps sulphate and chloride chemistries separate
- small autoclave and tanks fast leach kinetics
- optimizes selection of materials of construction
- fast production of metals and low lock-up of value





#### Lifezone Metals Hydromet - Comparison with Smelting









## Lifezone Hydromet Testwork - Metals Extraction Results

| GM-Au-Ni-Cu-Co Concentrate                       |   | Overall Recoveries into Solution (%)         |    |     |     |      |      |      |  |
|--|---|--|----|-----|-----|------|------|------|--|
| mple I   | ID Type                                   | Pt   | Pd | Rh  | Au  | Ni   | Cu   | Со   |  |
| Kabanga Nickel Scoping Test Results - Test 1 (1) |   | <u>,                                    </u> | -  | -   | - 5 | 98.5 | 96.9 | 97.5 |  |
| Kaba   | anga Nickel Scoping Test Results - Test 2 | 2  | -  |     |     | 99.7 | 99.6 | 99.8 |  |
| Α  | UG2                                       | 99   | 97 | 93  | 99  | 97   | 93   | 99   |  |
| В  | UG2                                       | 99   | 98 | 96  | 97  | 95   | 96   | 83   |  |
| C  | Merensky                                  | 99   | 98 | 97  | 99  | 99   | 99   | 98   |  |
| D  | UG2-Merensky                              | 99   | 98 | 96  | 99  | 98   | 99   | 93   |  |
| E  | Platreef                                  | 99   | 98 | 96  | 99  | 99   | 99   | 99   |  |
| F  | Platreef                                  | 98   | 99 | 97  | 96  | 99   | 99   | 99   |  |
| G  | Polymetallic Great Lakes                  | 97   | 99 | 95  | 96  | 99   | 99   | 99   |  |
| Н  | Polymetallic Great Lakes                  | 99   | 99 | -   | 99  | 99   | 99   | 99   |  |
| 1  | UG2-Merensky                              | 99   | 98 | 90  | 99  | 97   | 96   | 95   |  |
| J  | Polymetallic North America                | 95   | 99 | -   | 99  | 99   | 99   | 98   |  |
| K  | Great Dyke                                | 99   | 98 | 95  | 98  | 98   | 98   | 96   |  |
| L  | Great Dyke                                | 99   | 98 | 89  | 99  | 99   | 99   | 96   |  |
| M  | Polymetallic Australia                    | 99   | 99 | -   | 92  | 99   | 99   | 93   |  |
| N  | Platreef                                  | 98   | 99 | -   | 97  | 99   | 99   | 99   |  |
| 0  | Platreef                                  | 97   | 93 | 93  | 94  | 99   | 99   | 98   |  |
| Р  | Platreef                                  | 99   | 98 | 94  | 97  | 99   | 99   | 98   |  |
| Q  | Ni-Cu-Co Sulphide                         | -  | -  | -   | -   | 98   | 99   | 99   |  |
|  | Mean                                      | 98   | 98 | 94  | 97  | 98   | 98   | 96   |  |
| ı-Ag-Cı  | u-Co-Zn-Pb-Sb Concentrate                 | Overall Recoveries into Solution (%)         |    |     |     |      |      |      |  |
| ample I  | ID Type                                   | Au   | Ag | Zn  | Pb  | Cu   | Co   | Sb   |  |
| 1  | High-grade carbonaceous polymetallic ore  | 91   | 95 | 99  | 95  | 98   | -    | -    |  |
| 2  | Refractory gold concentrate               | 96   | -  | -   | 81  | 98   | 97   | -    |  |
| 3  | Refractory gold polymetallic concentrate  | 98   | 97 | 99  | 97  | 99   | -    | 95   |  |
| 4  | Double refractory Cu-Au concentrate       | 98   | 98 | -   |     | 99   | -    | -    |  |
| 5  | Refractory gold concentrate               | 98   | 98 | -   | -1  | -    | -    | -    |  |
|  | Mean                                      | 96   | 97 | 100 | 96  | 99   | 97   | 95   |  |

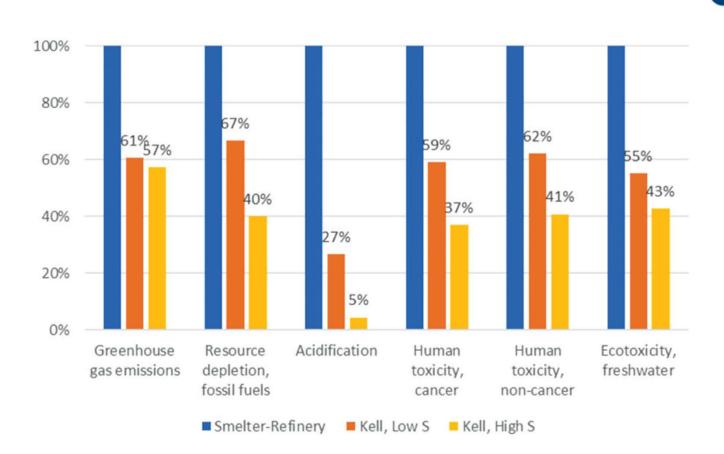
Source: Company Study by Liddell, K.S., Adams, M.D., Smith, L.A., and Muller, B Kell hydrometallurgical extraction of precious and base metals from flotation concentrates – Piloting, engineering, and implementation advances. Published in the Journal of the Southern African Institute of Mining and Metallurgy (2019). Testing was performed at Simulus Laboratories in Perth, Australia.

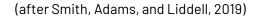






### **Comparison of Environmental Profiles**

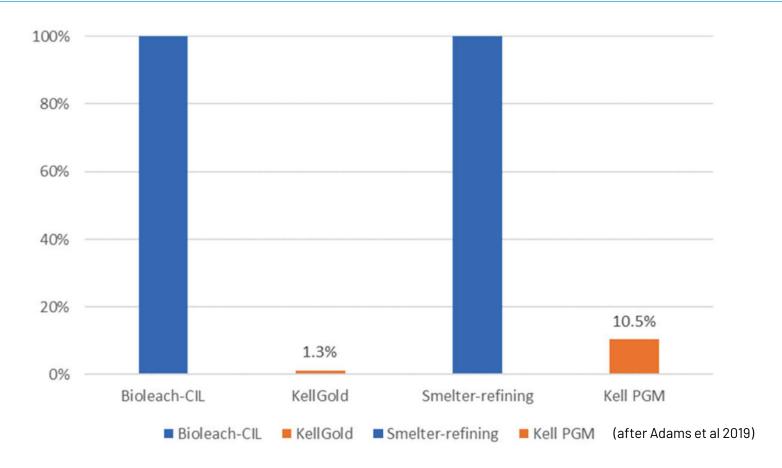








## Comparison of Working Capital Value Lockup (In-process Metal Inventory)







# Outlook

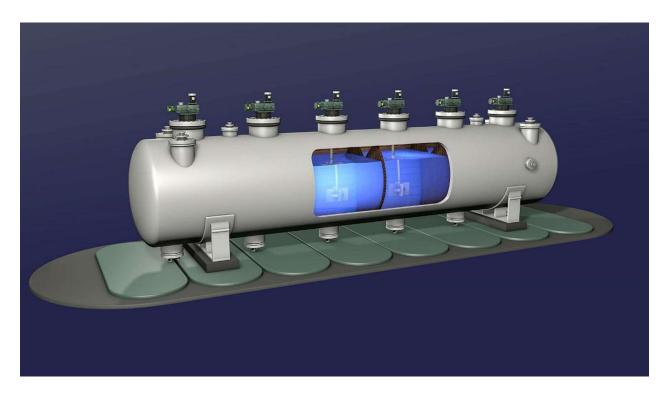
Chloride-Based Leaching Systems





### **Outlook for Chloride-Based Leaching Systems**

- Several chloride-based leaching systems have been tested in recent years at batch or pilot scale
- Lifezone Metals technology is at DFS or Detail Design stage for several commercial-scale applications
- Implementation of bulk chloride-based leaching systems at commercial scale is likely to take place in the next few years







## Acknowledgements

**Lifezone Metals** 

**Simulus Engineers & Laboratories** 







The supply chain solution for clean metals

